### **Technical Education and Analysis for Community Hauling and Anaerobic** Digesters (TEACHAD)

#### **TEACH AD Webinar Series - June 29, 2023**

Anaerobic Digestion: an overview of four technologies (CSTR, anMBBR, PFR, CLR) and their applications

RGY RESOURCES UIC CE ER

### Technical Education and Analysis for Community Hauling and Anaerobic Digesters – TEACH AD

The goal of this program is to help communities and water resource recovery facilities in the Midwest region divert food waste from landfills by providing education and no-cost technical assistance to explore the increased adoption of anaerobic digestion and renewable energy biogas technologies.

- Educational Assistance
- Technical Assistance

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# Webinar Speakers



#### **Marcello Pibiri**

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**Xavier Dhubert** 



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After the presentation you will receive a brief survey. We appreciate your feedback



Contact Sam Rinaldi at: samr@uic.edu or 312-996-2554 for assistance

# **Presentations**

# **Technical Issues**



# Importance of diverting food waste from landfills

- Municipal solid waste (MSW) landfills are the third-largest source of human-related methane emissions in the **United States**
- By reducing the amount of food waste landfilled, we reduce methane emissions

Manure Management 10%

Other Landfills 2%

#### 2018 U.S. Methane Emissions, By Source



Note: All emission estimates from the Inventory of U.S. Greenhouse Gas Emissions and Sinks: 1990-2018. U.S. EPA. 2020.



#### Importance of diverting food waste from landfills

- One-third of all food produced for human consumption worldwide is lost or wasted
- Source Reduction
- Feed People, Not Landfills
- Industrial Uses
  - Anaerobic digestion



#### **Food Recovery Hierarchy**

Source Reduction Reduce the volume of surplus food generated

Feed Hungry People Donate extra food to food banks, soup kitchens and shelters

> Feed Animals Divert food scraps to animal food

Industrial Uses Provide waste oils for rendering and fuel conversion and food scraps for digestion to recover energy

> Create a nutrient-rich soil amendment

Landfill/ Incineration Last resort to disposal



# **Overview of anaerobic digesters**

 Anaerobic digestion is the natural process in which microorganisms break down organic materials in the absence of oxygen.



- Biogas
- Digestate



#### Sources: U.S. Environmental Protection Agency

#### CENTER ENERGY RESOURCES

# SEBIGAS

![](_page_8_Picture_1.jpeg)

**Energy Resources Center** 

![](_page_8_Picture_3.jpeg)

#### **ANAEROBIC DIGESTION TECHNOLOGIES AND THEIR APPLICATIONS: SEBIGAS SOLUTIONS**

#### Technical Education and Analysis for Community Hauling and Anaerobic Digesters **TEACH AD**

![](_page_8_Picture_6.jpeg)

# **Presentation Outline**

- Forewords
- Anaerobic digestion advantages
- Continuous Flow Stirred Tank Reactors CSTR in agriculture RNG & in organic waste projects
- anaerobic Moving Bed Bio Film Reactors anMBBR

technology in industrial plants

- Plug Flow Reactors (PFR),
- Covered Lagoon Reactors (CLR)
- Co-digestion
- Conclusion

![](_page_9_Picture_10.jpeg)

#### Anaerobic digestion, not a new idea, but aligned with the challenges of our time

Theses days the energy business is mostly lead by Tax Credits, Financing, Public Opinion, and more recently by Carbon Accounting than by technologies. Examples are many in hydrogen, carbon capture, energy storage, syngas, biocoal, ....

Biogas production from waste through anaerobic digestion was originally use to dry digestate or to produce electricity. In the US the industry started by going the injection in natural gas pipeline. Now with potential changes in tax credits, electricity generation for EV might be in play?

If one add the numerous claims of companies whose sole purpose is "to save the world" in almost every field from water electrolysis to energy storage, to concentrated solar, ... it is no wonder that industrial companies have trouble establishing a decarbonation plan for the coming 30 years.

The solution is to get started on sound projects, which make both economical and technological sense on their own.

 $\rightarrow$  Biogas production from waste streams with enough organic content fits this approach.

![](_page_10_Picture_6.jpeg)

- -in Europe over 20 years ago rNG way with

# Example of XXI century anaerobic digestor plantSEBIGAS **INDUSTRIAL PLANT**

![](_page_11_Picture_1.jpeg)

Xalastra is an anaerobic digestion plant located in Salonicco (Greece) built in 2017. It consists of two digestors and structured in order to process heterogeneous and **complex biomasses** . The plant has a pre-treatment phase of by-products consisting of a sanitization and pasteurization system. At the end, digestate undergoes on a specific water treatment .

The plant processes 148 tons of by -products daily, divided into cattle manure, slaughter waste, expired food, beer residues and whey. The plant has an installation power of 1 MWe and produces 450-500 Nm3/h of biogas .

At the same time, it **reduces costs** in the waste the disposal.. Furthermore, for circular economy, they reuse of digestate as a fertilizer and soil improver in the surrounding areas.

**CLIENT NAME:** 

LOCATION:

FEEDING:

**INSTALLED POWER:** 

Xalastra

Salonicco (Greece)

Cattle manure, slaughter waste, expired food, beer residues, whey

1 MW e

#### CLIENT

#### THE PLANT

#### THE RESULT

Thus Xalastra, valorizes waste by producing electricity, that is reused in their production cycle.

#### NOTE: 1 MWe, the maximum limit to receive subsidies!

### Example of XX century anaerobic digestor SEBIGAS

Project of a Modern Drying Unit with a Combination of Methanization and Combustion of Solid Waste

![](_page_12_Figure_2.jpeg)

The technology is proven. On a personal note, that was my first project after my engineering school in 1983.

![](_page_12_Picture_4.jpeg)

VIEW OF THE DIGESTOR AND THE TECHNICAL ROOM (Figure No.3) FOLLOWING INSTALLATION

![](_page_12_Picture_6.jpeg)

(Figure No.5) INSIDE OF THE DIGESTOR MIXER AND SCRAPER DEVICE

![](_page_12_Picture_8.jpeg)

![](_page_12_Picture_9.jpeg)

![](_page_12_Figure_10.jpeg)

Image: private collection

### **Anaerobic digestion Technologies**

![](_page_13_Figure_1.jpeg)

![](_page_13_Figure_3.jpeg)

![](_page_13_Figure_4.jpeg)

#### ANAEROBIC DIGESTION TECHNOLOGY ADVANTAGES

![](_page_14_Picture_1.jpeg)

 $C0^2$ 

Brings sustainability and circularity in the production cycle

Our 84 plants in operation since 2010 led us achieve these goals:

23

Produces good quality fertilizers, soil improvers and energy from renewable resources

### SEBIGAS

#### **76 MWe INSTALLED**

#### 23.000.000 TONS CO<sub>2</sub> EQ. AVOIDED

#### TECHNOLOGY

Anaerobic digestion is a **BIOLOGICAL PROCESS that takes** place in the ABSENCE OF OXYGEN and thought which the organic content of biomass is transformed into biogas.

The biomasses used as inputs are diverse and come from the agricultural, industrial, waste or sludge management sectors.

#### ENERGY

0

After appropriate treatments, biogas can be used to produce electricity and thermal energy from cogeneration, or separated to obtain biomethane and carbon dioxide for industrial used.

The digestate leaving the process serves a dual purpose in agronomic terms, as it makes mineral elements available to plant and contributes to carbon storage in our soils. The digestate output can be separated and, if necessary, undergoes specific post -treatments.

#### **PROCESS**

#### DIGESTATE

![](_page_15_Picture_9.jpeg)

#### Acronyms, Parameters, and Definitions,

#### Acronyms

- ATA anaerobic toxicity assays, a variety of chemical compounds that can inhibit digestion and especially CH4 formation, such as chlorinated compounds,
- <u>BMP</u> biochemical methane potential, The potential to produce biogas from an organic waste
- <u>BOD</u> biochemical oxygen demand; <u>COD</u> chemical oxygen demand
- HRT hydraulic retention time, the average length of time the dissolved portion of the waste spends in the digester.
- <u>SRT</u> solids retention time, the average length of time the feedstock remain in the digester's reactor and remain in contact with the bacteria. SRT & HRT are not always equal.
- <u>Psychrophilic</u>, ambient temperature; <u>Thermophilic</u> Digestion at 50 –60 ℃.. <u>Mesophilic</u> Digestion at 25–40 ℃.
- OLR organic loading rate indicates the amount of VS that can be fed into the digester per day in g VS/L/day
- <u>TS</u> total solids, weight of the substrate after drying as percentage of wet weight. Also called dry matter ( DM)
- VFA volatile fatty acid
- VFA/Alkalinity Ratio\_, Indicates the progress & stability of the digestion, and is used for process control. A ratio of 0.1 -0.25 is ideal and 0.5 indicates a sour digester
- <u>VS</u> volatile solids, the fraction of TS that are combustible and are used as an estimate of organic matter content.
- Loading rate Amount of substrate added to the digester. Expressed as kg VS per m3 digester and day.
- <u>C/N quota</u> Relation between carbon and nitrogen content in the substrate.
- Methane yield Amount of produced methane expressed e.g. Nm3 per ton TS.

- Agitation or not, type of natural, hydraulic, digestate recirculation, mechanical (several types) • Heated or not, type of heating from the wall, external
- recirculation,
- Hybrid options,
- Pre-digestion

- Retention time
- Temperature
- Characteristics of volatile solids (VS)
- Inhibitors

- pH,
- total gas volume and gas composition, methane, hydrogen, carbon dioxide and hydrogen sulfide.
- FOS/TAC (volatile organic/(fatty) acids/total inorganic carbon)
- Ammonium -nitrogen concentration,
- solid and volatile solid of digestate,

# 

Key Anaerobic Digestor Features:

Parameters that determine the efficiency of converting organic

- materials to biogas
- Organic loading rate (OLR)

Some parameters measured to evaluate a reactor performances & stability

#### The four main Anaerobic Digestion technologies

#### **CSTR**

DRY SUBSTANCE	5% < DS < 10%	DRY SUBSTANCE	DS < 1%
THERMAL REGIME	Mesophilic or thermophilic	THERMAL REGIME	Psychrophilic or mesophilic
RETENTION TIME	20 < days < 60	RETENTION TIME	< 10 days
MIXING SYSTEM	Mechanical (slow and fast mixers), inside the reactor	MIXING SYSTEM	Mechanical (slow mixers) inside the reactor - gasmixing

#### **CLR**

DRY SUBSTANCE	DS < 5% and low fibre content	DRY SUBSTANCE	15% < DS < 35%
THERMAL REGIME	Psychrophilic or mesophilic	THERMAL REGIME	Mesophilic or thermophilic
RETENTION TIME	15 < days < 25	RETENTION TIME	20 < days < 60
MIXING SYSTEM	Hydraulic mixing (recirculation pumps)-gasmixing	MIXING SYSTEM	Mechanical (slow mixers) inside the reactor

![](_page_17_Picture_5.jpeg)

# SEBIGAS

#### anMBBR

#### **PFR**

### **Covered Lagoon Reactors (CLR)**

It is the simplest of the digestors' designs, however, still require experiences to be properly designed and built.

The anaerobic digestion of the organic content occurs through the biomass recirculation in an active sludge layer, with controlled quantities and velocities.

#### ADVANTAGES:

- Perfect internal mixing and optimized contact between the fresh biomass and the active sludge
- large internal buffer capacity and high process stability
- Very flexible automated feed distribution inside the anaerobic reactor, avoiding local biological disturbances
- Effluent clarification and flexible sludge recycle/discharge
- Flexible extraction of surplus biosolids from the lagoon reactor

![](_page_18_Picture_9.jpeg)

![](_page_18_Figure_10.jpeg)

### SEBIGAS

#### Image: private collection

### **Plug Flow Reactors (PFR)**

- It is a versatile technology that present a few variants, not continuously mixed, but either mechanically (paddles), or with the biogas re -circulation some forced movement of the material is possible,
- Due to the shape (elongated rectangle) and the feeding to one side and the outflow from the other side, it is a first in/first out type. The 4 stages of anaerobic digestion are somewhat sequential and separated
- The biogas is collected in inflatable
- It is often found at large dairy farms and It can accommodate some mixed waste input

![](_page_19_Figure_5.jpeg)

![](_page_19_Picture_6.jpeg)

Image: Web – Science Direct & Research Gate

### SEBIGAS

Image: private collection

### CSTR TECHNOLOGY IN BIGESTER AGRICULTURERRIG PROJECTS

SEPARAT

OR

DIGESTAT E STORAGE TANKS

CSTR = Continuous Flow Stirred Tank Reactor SILAGE

### SEBIGAS

SOLID FEEDER

COGENERATI ON UNIT

# AGRICULTURE RNG

Specific pretreatments solutions are implemented to digest complex matrices (sanitization, pasteurization, sand removal)

 Pasteurization or flotation technologies may
be implemented in case of complex matrices (ex. slaughterhouse waste)

 $\sim$ 

Post-treatments step for digestate valorization and nitrogen recovery can be considered

![](_page_21_Picture_5.jpeg)

![](_page_21_Figure_7.jpeg)

#### AGRICULTURE RNG ADVANTAGES

![](_page_22_Picture_1.jpeg)

 $C0^2$ 

An agricultural plant with an installed power of 2 MW and fed with around 66.000 t/ y of various biomasses

(maize silage, triticale silage, cow and pig manure, poultry litter)

In operation for 12 years, can avoid around 890.000 tons CO <sub>2</sub> equivalent

Produces good quality fertilizers, soil improvers and energy from renewable resources

![](_page_22_Picture_6.jpeg)

# CSTR TECHNOLOGY IN

N.

T A

Feeding: 50.000 t/y of MSW

+ 5.000 t / y of green waste

# SEBIGAS

9

#### **ORGANIC WASTEPLANTS**

The plant ensures high performance while digesting high volumes and heterogeneous biomasses

Pretreatments to remove any unwanted contents that could affect the anaerobic digestion process (opening of bags, sieving and sand removal, removal of metals, etc.)

![](_page_24_Figure_3.jpeg)

### SEBIGAS

![](_page_24_Figure_5.jpeg)

![](_page_24_Picture_6.jpeg)

SOLID

FRACTION

# ORGANIC WASTE

![](_page_25_Picture_1.jpeg)

£s

It recovers 50.000 tons of organic waste to produce 650 Nm3/h of biomethane

**1.700 TOE** (Tons of Oil Equivalent) are saved every year

**10.000 t/y of quality compost**, used as a fertilizer + 30.000 m 3/ y of clean effluent, suitable for river discharge

Biomethane produced (> 5,000,000 Nm3/ year) for transportation is equal to 180.000 car fill up, to travel more than **54.000.000 km** 

![](_page_25_Picture_6.jpeg)

#### Typical large plant with CSTR digester, for the organic fractions of MSW

![](_page_26_Figure_1.jpeg)

#### TABLE OF CONTENT

- **RECEIVING HALL PRETREATMENT EQPM**
- GRIT REMOVAL SYSTEM 2.
- **BUFFER TANK** 3.
- DIGESTER (CONCRETE 23X11) 4.
- PUMPING STATION 5.
- POST-DIGESTER 6
- CENTRIFUGAL DECANTER 7.
- **BIOLOGICAL AEROBIC REACTOR** 8.
- UF AND RO AREA 9.
- 10. EVAPORATOR
- 11. BIOGAS DESOX AND DEHUMIDIFICATION
- 12. BIOGAS UPGRADING AND HP COMPRESSOR

REMARK: COMPOSTING AND AIR TREATMENT IS MISSING!!!!

ultrafiltration (UF) and reverse osmosis (RO)

# SEBIGAS

Site optimization and consideration to foot -print constrains is important.

Especially in the case of more complex plants where the digesters themselves are only a portion of the overall process, with pre -digesters and post-digesters requirement.

Presented here is a 1200 Nm3/h of biogas From 140 ton/d of domestic waste.

#### **Typical Key Values**

![](_page_27_Picture_1.jpeg)

Digester (CSTR) can be up to 32 m in dia. 10 m height for a volume of 7400 m3

CSTR digester retention time is usually 30 days (varies from 15 to 30)

Such digester could produce different flow of biogas of biogas (depending on the feedstock): for example:

1 ton of liquid cow manure could produce between 15 and 25 Nm3 of gas

![](_page_27_Picture_6.jpeg)

1 ton of waste from slaughterhouse could produce 200 and 225 Nm3 of gas

NOTES: Use 10 kWh/Nm3 of CH4 for LCV as a rounded number 1,000 cows produce 1 ton manure per hour

![](_page_27_Picture_10.jpeg)

![](_page_27_Picture_11.jpeg)

# anMBBR TECHNOLOGY INDUSTRE PLANTS

CAULINN BE'LIGH

aerobic Moving Bed Biofi

### a nMBBR REACTOR

# Which biomasses can be digested in the anMBBR Reactor?

![](_page_29_Picture_2.jpeg)

![](_page_29_Picture_3.jpeg)

It's a tech industria Allows a low dige

![](_page_29_Figure_5.jpeg)

- It's a technological solution for the treatment of
- industrial waste water in anaerobic digestion.
- Allows an on-site management of high streams, with low digestion volumes.

RY FANCE	DS<1%
RMAL IME	psychrophilic (or mesophilic (38-43°)
NTION //E	<10 days
ING TEM	Mechanical (slow mixers) inside the reactor - gasmixing

![](_page_30_Picture_0.jpeg)

### a nMBBR REACTOR

Virgin plastic elements called "Carriers" are inserted into the reactor. Their shape ensures a high surface support for the proliferation of bacteria, allowing the creation of biofilm and enabling the digestion process

![](_page_30_Picture_3.jpeg)

![](_page_30_Picture_4.jpeg)

![](_page_30_Picture_5.jpeg)

# anMBBR industrial plants

The plant ensures high performance while digesting high volumes and heterogeneous biomasses

![](_page_31_Picture_2.jpeg)

It is an alternative solution for energy -intensive sectors.

![](_page_31_Picture_4.jpeg)

![](_page_31_Picture_5.jpeg)

### ANMBBR INDUS TRIAL PLANTS

CAUTION BE"TIGH

It contributes to the production of energy to be directly used in the production cycle

Reduces the volume and sludge disposal costs

The plant valorises high volumes of effluents, alternatively sent to disposal

The plant is a source of saving, considering the energy demand of these industrial sectors

![](_page_32_Picture_5.jpeg)

#### **Co-Digestion**

SEBIGASuses a combination of expertise, research and flexibility to create a tailor made mass balance and treat in anaerobic digestion heterogeneous and complex biomasses.

With a portfolio of more than **70 types of biomass** analyzed, SEBIGAS guarantees the full exploitation of every biomass used as a feeding.

![](_page_33_Figure_3.jpeg)

### SEBIGAS

![](_page_33_Figure_5.jpeg)

![](_page_33_Picture_6.jpeg)

![](_page_33_Picture_7.jpeg)

![](_page_33_Picture_8.jpeg)

#### agro-industrial liquid effluent and by-products

dairy production, alcoholic beverages, soft drinks, sugar mills, paper mills, roasting, ethanol, oil, rice...

#### sludge

from municipal wastewater and industrial wastewater treatment plants

#### slaughterhouse waste

fats, animal meal, rumen and stomach contents, offal, blood...

#### OFMSW

Organic Fraction of Municipal Solid Waste

#### Containerization

The important point of cost is to be considered. Especially in the US with supply chain disruptions, and labor force shortage and generally high cost, projects should focus on standardization and modularity.

BIOMASS FEEDING PUMPING STATION

![](_page_34_Picture_3.jpeg)

![](_page_34_Picture_4.jpeg)

![](_page_34_Picture_5.jpeg)

To cut 50% time and site work, Sebigas offers the entire pumping system (feedstock feed, digestate extraction, recirculation, transfer, ...). all installed in containers for "plug and produce" installation. Container arrives already tested and ready for commissioning.

![](_page_34_Picture_8.jpeg)

### Conclusions

In general, the strength and weakness of the American approaches to industrial project is the search for standardization, "cookie cutter" projects to eliminate technical risks, better access to finance, shorter project time from permitting to erection & commissioning. Thus, the specialization of companies and the mono-feedstock approach, mainly dairy farms and in addition, the search for the largest possible projects.

Universal is the search and need for subsidies, the RINs in the US, the fixed rNG or r-electricity in Europe. However, when all the large farms are equipped with a biogas plant, remaining projects will have to be smaller and more diversified. Thus, the European experience with co-digestion of various feedstocks.

In general, animal manures digest (or bio -degrade) more slowly than other organic matter. The addition of co-digestion feedstocks can increase the biodegradability and the VS in the digester. Volatile solids are the digestible organic matter that can be converted into methane gas. An increase in VS means an increase in biogas and methane production. Some crop residue feedstocks that contain a significant amount of lignin (which is not digestible) may be difficult to break down in the digester.

That approach often requires pre-treatment such as sorting, shredding, and dilution, ..also mixing would be important to feed the digester as homogeneous product as possible, which might require a holding tank upstream of the digesters. There is more frequent requirement for pH adjustment. Laboratory testing Tecomes a pre-requisite to any serious project. tests might include a biochemical methane potential (BMP) test, anaerobic toxicity assays (ATA), total solids, volatile solids, alkalinity (or pH), and chemical oxygen demand (COD

![](_page_35_Figure_5.jpeg)

#### Conclusions

Either co-digested or not, the broader types of feedstocks require to consider different types of digestor, each one better suited for a given project. Sebigas focuses on:

- Continuous Flow Stirred Tank Reactors (CSTR), The most versatile, easily arranged in multiple digesters. TS between 5% & 10% (feedstock can be diluted
- Anaerobic Moving Bed Bio Film Reactors (anMBBR), Perfect for any feedstock with TS below 1%, thus more waste -water treatment applications.

Some more recent developments are:

- The shifting or not depending on tax credits, regulations, and incentives, from rNG (biogas upgrading to produce natural gas quality fuel) production to electricity production through RICEs (Reciprocating) Internal Combustion Engines) or CHP (Combined Heat & Power),
- The CCUS Carbon Capture Utilization & Storage. Biogas is mainly methane (50 –75%) and carbon dioxide (25–50%). Up to recently CO2 would be vented. Although relatively small quantity when compared to a steel or cement plant (0.5 to 1 Mon ton CO2 emitted / year) as the technologies and infrastructure continue to grow, another benefit of the anaerobic digestion will be added

- $CO_2 CO_2 CO_2 CO_2$
- WHATEVER YOUR CO<sub>2</sub>!

UIC ILLINOIS CHICAGO

Energy Resources Center

Technical Education and Analysis for Community Hauling and Anaerobic Digesters

# **SEBIGAS**

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SEBIGAS RENEWABLE ENERGY SRL www.sebigas.com

![](_page_37_Picture_7.jpeg)

**TEACH AD** 

# **THANK YOU!**

#### HEADQUARTER

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# **TEACH AD – Educational Assistance**

- In person workshops (2)
  - **Onsite events**
  - Tour of the site
  - **April 2022: Kishwaukee Water Reclamation District**
  - May 2023: Green Era Campus
  - Visit erc.uic.edu/bioenergy/teachad/in-person-workshops/
- Webinars (10)
  - Cover different aspects of an anaerobic digestion project
  - Visit <a href="mailto:erc.uic.edu/bioenergy/teachad/teach-ad-webinars/">erc.uic.edu/bioenergy/teachad/teach-ad-webinars/</a>
- Project profiles (8)
  - UW Oshkosh, Urbana Champaign Sanitary District, Kishwaukee WRD, St. Cloud Nutrient, Energy and Water (NEW) Recovery Facility, Barstows Longview Farm, Des Moines **Metropolitan Wastewater Reclamation Authority, Green Era**
  - Visit <a href="https://erc.uic.edu/bioenergy/teachad/project-profiles/">https://erc.uic.edu/bioenergy/teachad/project-profiles/</a>

![](_page_38_Picture_14.jpeg)

# **TEACH AD – Technical Assistance**

- Anaerobic Digestion Technical Assessments
  - Tailored technical assistance to each client
  - Initial economic and physical feasibility assessment for (co)digestion of organic wastes
  - Assess opportunity for using U.S. EPA's Co-Digestion Economic Analysis Tool (CoEAT)
  - Report presentation and follow up with next steps

![](_page_39_Figure_6.jpeg)

**USER'S MANUAL: CO-DIGESTION ECONOMIC** ANALYSIS TOOL

![](_page_39_Picture_11.jpeg)

#### GY RESOURCES

# **TEACH AD – CoEat Analysis**

	Current	Future A	Future B	Future C	Future D	
Biogas Produced (cf/yr)	13,862,185	26,169,378	26,169,378	26,169,378	26,169,378	37,978.59 cfd
Total Biogas Heating Energy (MBTU/yr)	6,307	11,906	7,620	11,906	0	71,696.92 cfd
Total Energy Needed for Heating (MBTU/yr)	3,853	4,421	4,421	4,421	4,421	49.7895311 cfm
Max Capacity of Digester (gal)	1,115,000	1,115,000	1,115,000	1,115,000	1,115,000	
Feedstock Feed Rate (gal/day)	13,215	16,907	16,907	16,907	16,907	Return to Inputs/ GUI
% Solids of Feedstock Fed to Digester (%)	3.8%	5.2%	5.2%	5.2%	5.2%	
Percent Volatile Solids Reduction (%)	57%	57%	57%	57%	57%	
Actual Hyraulic Retention Time (days)	67.8	53.0	53.0	53.0	53.0	Restore Default Formulas
Target Hydraulic Retention Time (days)	15.0	15.0	15.0	15.0	15.0	
Available Capacity (Gal/day)	46.519	42.827	42.827	42.827	42.827	
Additional Volume Needed to Treat Feedstock (gal)	0	0	0	0	0	Print Input Values
Mass of Biosolids (Tons/yr)	450	704	704	704	704	
Biosolids Cost (\$/yr)	(\$58 <i>,</i> 608.55)	(\$88,792.80)	(\$88,792.80)	(\$88,792.80)	(\$88,792.80)	
Biosolids Revenue (\$/yr)	\$0.00	\$0.00	\$0.00	\$0.00	\$0.00	
Tipping Fees (\$/yr)	\$0.00	\$127,622.25	\$127,622.25	\$127,622.25	\$127,622.25	
Avoided Natural Gas Costs (\$/yr)	\$33,995	\$66,038	\$28,222	\$0	(\$39,006)	
Avoided Electricity Costs (\$/yr)	\$0	\$0	\$129,613	\$0	\$0	
Avoided Vehicle Fuel (\$/yr)	\$0	\$0	\$0	\$305,983	\$486,629	
Annualized Cost of Plant Upgrades (\$/vr)	\$0	(\$36.833)	(\$113.230)	(\$134.973)	(\$149.467)	
Annual Operations and Maintenance (\$/yr)	(\$5,000)	(\$5,000)	(\$67,566)	(\$87,632)	(\$121,673)	
Net Annualized Value (\$/vr)	(\$29.614)	\$63.035	\$15 860	\$122.208	\$715 217	
	(723,014)		\$13,005 	,2122,200 = 0	Υ <u>΄</u> Ι,3Ιζ	
Simple Payback (yr)	NA	NA	7.7	5.8	4.9	

#### **NERGY RESOURCES** UIC ER

# **TEACH AD – CoEat Analysis**

**Current:** Use biogas to heat digester and incomming feedstock. Value is given to excess heat. If digester heating demand is not met, expense for natural gas will incur.

Future A: Use biogas to heat digester and incomming feedstock. Value is given to excess heat. If digester heating demand is not met, expense for natural gas will incur. This scenario is not achievable as the plant does not have enough heat demand.

Future B: Use biogas in CHP to heat digester and incomming feedstock and generate electricity. Value is given to the electricity generated and excess heat. If digester heating demand is not met, expense for natural gas will incur.

Future C: Use biogas to heat the digester and convert the rest to vehicle fuel. If digester heating demand is not met, no biogas will be available for CNG and an expense for natural gas will incur.

Future D: All biogas is converted into vehicle fuel. Cost of natural gas to meet the heating demand of the digester and incomming feedstock will incur.

For a detailed review of the calculations and assumptions, please observe the "4. Biogas Use" worksheet.

Analysis				
	Percent increase in heating demand =	g demand = 14.7%		
	Percent increase in biogas production =		88.8%	
	Percent increase in biosolids =		56.3%	
	Additional volume needed to treat feedstock =		None	[ga
	Size of CHP =		149	kW

![](_page_41_Picture_11.jpeg)

# **TEACH AD – EPA Food Waste Map**

Find address o	er place Q			
F R C	Near Me     Search for an address or locate on map     1301 Sycamore Rd, Dekalb, IL, 60113     Show results within 10 Miles     Show results within 10 Miles     O     Correctional Facilities     Educational Institutions     Healthcare Facilities     Hospitality Industry     Food Manufacturers and Processors	$5, \times \mathbf{Q}$ $\bigcirc$ 100 (1) > (29) > (2) > (15) > (9) >	C Set 1 D ekalb z	Sycamore earch result 301 Sycamore Rd, Dekalb, Illinois, 601 Coom to Cortiland
4mi			ESTI, N	ERE, Garmin, USGS, EPA, NPS US E

![](_page_42_Picture_2.jpeg)

#### CENTER ENERGY RESOURCES

# **TEACH AD - Contact**

#### **Marcello Pibiri**

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![](_page_43_Figure_3.jpeg)

![](_page_43_Figure_4.jpeg)

![](_page_43_Picture_5.jpeg)

### Questions

![](_page_44_Picture_1.jpeg)

#### Marcello Pibiri

**Senior Research Engineer UIC Energy Resources Center** 

![](_page_44_Picture_4.jpeg)

**Sr. Consultant North America** SEBIGAS RENEWABLE ENERGY

**Xavier Dhubert** 

![](_page_44_Picture_7.jpeg)

# TEACH AD Webinar Series Thank you for attending this webinar series. Let's keep in touch!

![](_page_45_Picture_1.jpeg)

# **Thank You** Please fill out our survey.

A recording of today's webinar will be posted, and you will be emailed a link by early next week.

![](_page_46_Picture_2.jpeg)

![](_page_47_Picture_0.jpeg)

# Thank You

![](_page_47_Picture_2.jpeg)